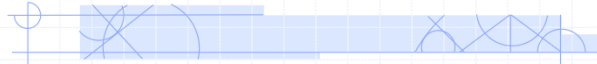




**ENGR 83 Final Project:**  
Affordable Flowmeter for Measurement of Low-Flowrate  
Suspended-Particulate Flow



Julian Leland  
ENGR 83, 2011  
Swarthmore College





# Presentation Outline

- Introduction
- Design Process
- Testing & Results
- Conclusion





# Introduction

- Problem: build a flow meter to measure volumetric flow through a hookah



[http://www.languageflowers.org/wp-content/uploads/2009/11/hookah\\_setup\\_diagram.pdf](http://www.languageflowers.org/wp-content/uploads/2009/11/hookah_setup_diagram.pdf)



# Introduction

- Goals
  - Measure flow rate to within  $\pm 10\%$ 
    - Instantaneous output
  - Total cost  $\leq \$100$
  - Long-term reliability of system.
- Constraints
  - Low flow velocity/flow rate
  - Gas with suspended particulate matter
    - “Sticky”/corrosive particulate
  - Can’t impede flow



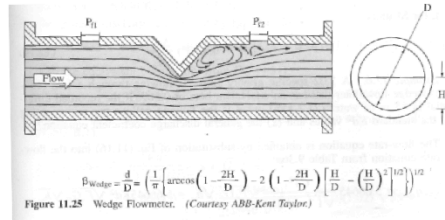
# Design Process

- Step 1: Problem Identification
  - Flow Characteristics
    - Dirty flow with “sticky” particulate
    - Low flow rate – mean flow of 12.9 lpm =  $2.15 \times 10^{-4} \text{ m}^3/\text{s}$  (Shihadeh)
    - Low Reynolds numbers – between 1000 and 3000
  - Meter Characteristics
    - VERY low allowable pressure differential – under .1 kPa (.014 PSI) or use will be interfered with (Shihadeh)
    - Meter must be clog-resistant, easily cleaned, no moving parts
    - Meter must be corrosion-resistant



# Design Process

- Step 1 Results
  - Type of Flowmeter: Wedge-type Meter



Flow Measurement Engineering Handbook 11.35

- Differential pressure meter
- Simple construction
- Resistant to clogging, low pressure loss, functional with low Reynolds number



# Design Process

- Step 2: Analytic Design

	A	B	C	D	E	F	G	H	I	J	K	L
10	Design Location											
11	Design Location											
12	Design Location											
13	Design Location											
14	Design Location											
15	Design Location											
16	Design Location											
17	Design Location											
18	Design Location											
19	Design Location											
20	Design Location											
21	Design Location											
22	Design Location											
23	Design Location											
24	Design Location											

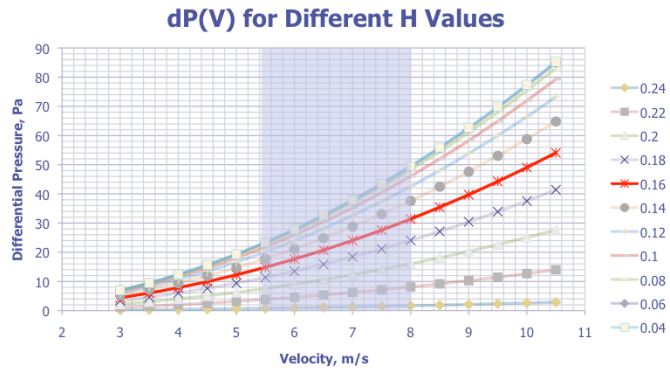
- Inputs: pipe diameter, opening height, fluid density, dynamic viscosity, flow velocity
  - Assumptions: Discharge coefficient is for .5" to 1" pipe
- Outputs: Flow rate, Reynolds number, beta ratio, expected differential pressure





# Design Process

- Step 2 Results



Mean expected flow region – between 5.5 and 8 m/s





# Design Process

- Step 2 Results

- Flow sensor: Sensirion SDP 1000-L025 Differential Pressure Sensor

- Bidirectional differential pressure sensor
- Analog output, logic level

- Range:  $\pm 62$  Pa (.0089 PSI)
- Resolution: .1 Pa ( $1.45 \times 10^{-5}$  PSI)
- Accuracy: .31 Pa ( $4.49 \times 10^{-5}$  PSI)

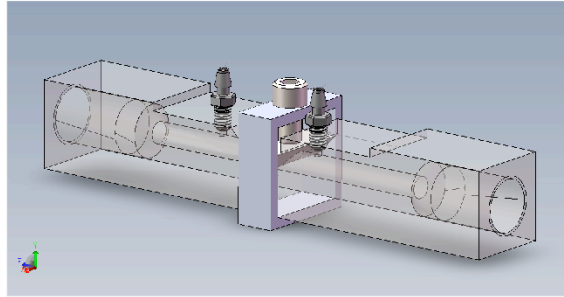
- For desired flow range, optimal H is .16"





# Design Process

- Step 3: Computer Simulation
  - Meter modeled in SolidWorks

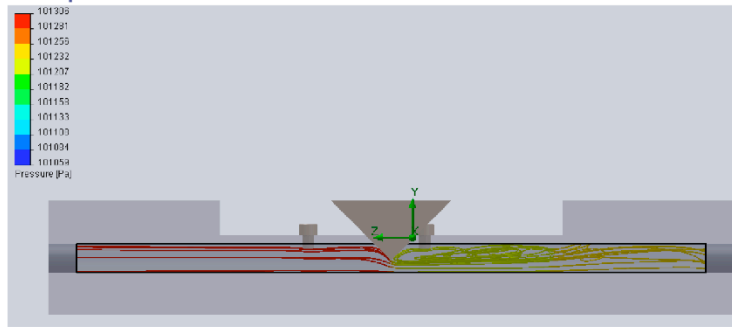


- Simulated in Solidworks Flow Simulation



# Design Process

- Step 3 Results



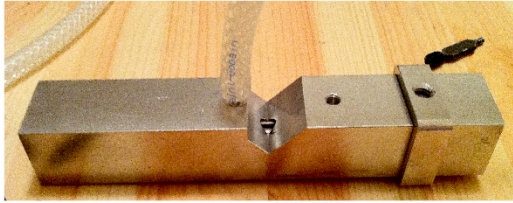
– Much higher dP: = 100 Pa at expected mean flow rate

However, not accurate simulation. Assumes atmospheric pressure at inlet and expected flow rate at output → does not account for pressure losses elsewhere in hookah, so assumes that they occur only in flowmeter. Consequently, simulation overestimates dP



# Design Process

- Step 4: Construction



Meter Body



Wedge Element

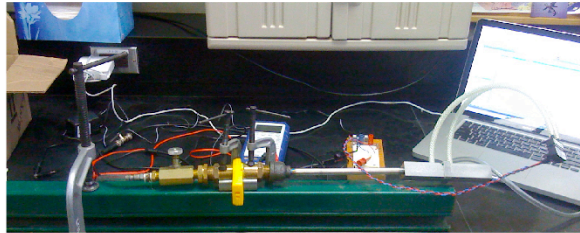




# Testing and Results

- Calibration

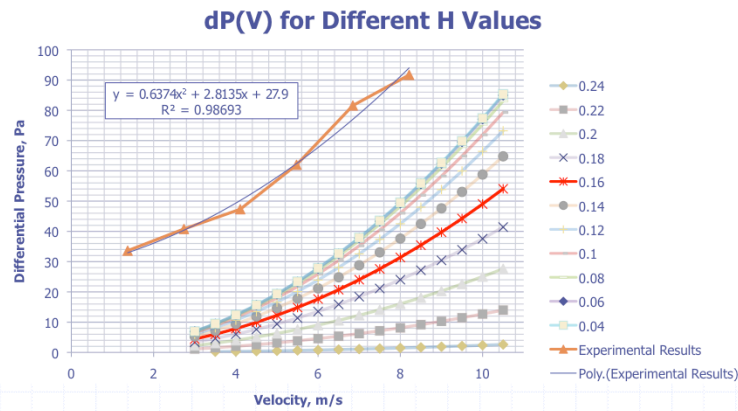
- Meter calibrated by placing meter in series with anemometer in known-diameter pipe
- Calibration possible between  $4.33 \times 10^{-5}$  and  $2.60 \times 10^{-4} \text{ m}^3/\text{s}$  – above, exceeds limits of sensor
- Test setup:





# Testing and Results

- Calibration Results



Exponential fit used because dP is function of velocity<sup>2</sup>

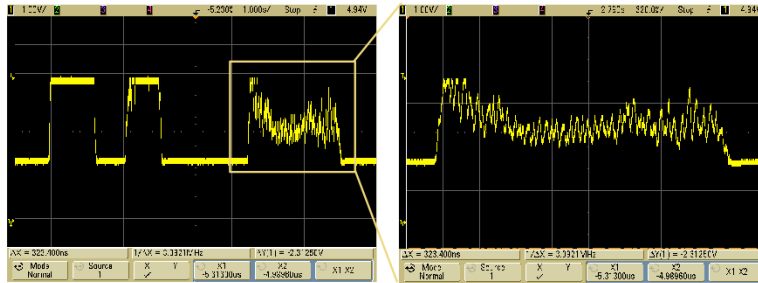
Significantly higher pressure differentials than expected – simulation results are much closer to accurate

Needed new flow sensor – appears to work better, but still possible to “max out”.  
Need to reanalyze what maximum flow rate is



# Testing and Results

- Other Tests
  - “Bubbling” signal noise – 11 Hz noise



- Does not interfere with signal - eliminated in software using LPF





# Testing and Results

- Results

- Goals:

- Cost: Flow sensor is \$90/unit – probably impossible to make for under \$100 unless sensor cost is reduced
    - Accuracy: impossible to test, need precise flow measurement device for ultra-low flows.
    - Long-term durability: to be determined through use

Initial results indicate that contamination of the sensor itself is unlikely to be a problem, but flooding of the pressure lines with hookah fluid may be.





# Testing and Results

- Future Work
  - Calibrate new sensor: ensure that sensor has not been damaged by handling
  - Implement contaminant traps for hookah fluid
    - Also reduce “bubbling” by providing vibration damper
  - Determine whether additional filtration is required
  - Implement more advanced “bubbling” filter in software



# Conclusion

Questions?

## References

- Miller, Richard W. *Flow Measurement Engineering Handbook*, 3<sup>rd</sup> Ed. McGraw Hill, 1996.
- Shihadeh, Alan. *A portable, low-resistance puff topography instrument for pulsating, high flow smoking devices*. [http://webfea.fea.aub.edu.lb/aerosol/downloads/MS-03-63\\_revised.pdf](http://webfea.fea.aub.edu.lb/aerosol/downloads/MS-03-63_revised.pdf)
- ———. *Towards a topographical model of narghile water-pipe café smoking: a pilot study in a high socioeconomic status neighborhood of Beirut, Lebanon*. <http://webfea.fea.aub.edu.lb/aerosol/downloads/topography.pdf>